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Method and adsorbant composition for <sup>82</sup>Rb generation.

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The present invention provides a composition comprising <sup>82</sup>Sr and an adsorbant selected from tin oxide, hydrated tin oxide, polyantimonic acid, titanium oxide, hydrated titanium oxide, ferric oxide and hydrated ferric oxide, and also provides a low <sup>82</sup>Sr breakthrough method of generating <sup>82</sup>Rb which comprises eluting such <sup>82</sup>Sr charged adsorbant.

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METHOD AND ADSORBANT COMPOSITION FOR  $^{82}\text{Rb}$  GENERATION

The present invention relates to a composition comprising  $^{82}\text{Sr}$  and an adsorbant selected from tin oxide, hydrated tin oxide, poly antimononic acid, titanium oxide, hydrated titanium oxide, ferric oxide and hydrated ferric oxide. This invention also provides a low  $^{82}\text{Sr}$  breakthrough method of generating  $^{82}\text{Rb}$  comprising eluting the  $^{82}\text{Rb}$  from the  $^{82}\text{Sr}$  charged adsorbant as described above.

Rubidium -82, a positron emitter with a half-life of 75-sec is readily obtainable from the parent Sr-82 ( $T_{1/2} = 25$  days). Rubidium can be used as a diffusible flow tracer for the myocardium and kidney, and as a nondiffusible tracer for brain blood flow. Serial injections of Rb-82 can be administered every 5 to 10 minutes by eluting (milking) Rb-82 from its 25-day Sr-82 parent. The advantages of Rb-82 are low radiation dose, ability to provide for repeated examinations every 5 minutes without constraints from body background, and a convenient and economical supply of a short-half-life positron emitter. (Yano et al., The Journal of Nuclear Medicine 20:961-966, 1979.)

Significant quantities of  $^{82}\text{Sr}$  are available for clinical investigation. The short-lived daughter, 75-second  $^{82}\text{Rb}$ , is of value in biomedicine for circulation and perfusion studies as well as for myocardial imaging as mentioned in U. S. Patent Number 3,953,567.

Loc'h et al. J. Nucl. Med. 21: 171-173, 1980 disclose a tindioxide ( $\text{SnO}_2$ )/HCl Ga-68 generator.

Arino et al. Int. J. Appl. Radiat. Isot. 29: 117-120, 1978 disclose a  $^{68}\text{Ge}/^{68}\text{Ga}$  radioisotope generator system which uses polyantimonic acid to selectively adsorb Ge and not Ga. The adsorption was speculated to be due to a dehydration reaction forming chemical bonding between Sb and Ge through oxygen.

Neirinckx et al. disclose titanium oxide in a generator for ionic gallium-68, see second International Symposium on Radiopharmaceutical Chemistry MRC. Oxford, 1978, p. 109.

Kopecky et al. Int. J. Appl. Radiat. Isot. 25: 263-268, 1974 disclose a  $^{68}\text{Ge}/^{68}\text{Ga}$  generator for the production of  $^{68}\text{Ga}$  in an ionic form. Aspects of the adsorption of carrier-free  $^{68}\text{Ge}$  and  $^{68}\text{Ga}$  on alumina,  $\text{Al}(\text{OH})_3$  and  $\text{Fe}(\text{OH})_3$  are discussed.

The present invention provides a composition comprising  $^{82}\text{Sr}$  and an adsorbant selected from tin oxide, hydrated tin oxide, polyantimonic acid, titanium oxide, hydrated titanium oxide, ferric oxide and hydrated ferric oxide, and also provides a low  $^{82}\text{Sr}$  breakthrough method of generating  $^{82}\text{Rb}$  which comprises eluting such  $^{82}\text{Sr}$  charged adsorbant. The eluent can be physiological saline or a buffered isotonic solution. The yields of  $^{82}\text{Rb}$  are high.

The method and compositions of the present invention result in eluates which are useful in positron imaging and in the subsequent measurement of blood flow through the myocardium, brain and kidneys. The present invention provides a small bolus size of 2-3 ml which is advantageous for lower volume per unit time infusion while maintaining an effective

amount of activity to monitor the patient.

The present invention is based on the discovery that breakthrough of Sr may be lowered by providing a particular adsorbant as described above, and preferably, tin oxide or hydrated tin oxide.

Hydrated tin oxide includes hydrated stannic oxide, hydrated stannous oxide, and mixtures of hydrated stannic oxide and hydrated stannous oxide. Preferably the hydrated tin oxide is amorphous. Tin oxide includes stannic oxide, stannous oxide and mixtures of stannous oxide and stannic oxide. Most preferably an amorphous mixture comprising tin oxide and a substantial amount (more than 10% by weight) of hydrated stannic oxide is used as the adsorbant.

The preferred adsorbant is in the form of chromatographic particles having an average diameter of 0.01 to 0.9 mm, and preferably, 0.05 to 0.1 mm.

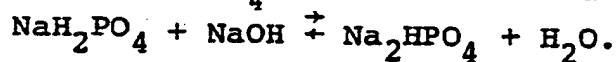
The eluent may be isotonic saline or isotonic saline buffered at physiological pH and may contain bacteriostat. Preferably a buffered eluent is used wherein the buffer may be a phosphate salt or a carbonate salt, preferably a phosphate salt. Most preferably, isotonic saline at physiological pH is used. Bacteriostats may be beneficially added to the eluent. Preferred bacteriostats are those which are pharmaceutically acceptable buffers, for example parabens.

The eluent is buffered at a pharmaceutically acceptable pH, preferably from pH 6.0 to pH 10 and most preferably, from pH 7.0 to pH 7.5. The concentration of the buffer in the eluent preferably is from .01 mmol to 200 mmol per liter of eluent solution.

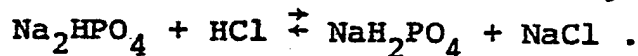
The saline concentration of the eluent is a pharmaceutically acceptable concentration. Preferably the saline is isotonic (0.9%).

Phosphate salts include alkali phosphates, alkaline earth phosphates, alkali metal hydrogen phosphates, alkaline earth hydrogen phosphates as well as hydrates of phosphate salts. Also phosphate salts include all phosphorous oxides which form phosphates upon addition to water.

A preferred phosphate salt is  $\text{Na}_2\text{HPO}_4$  which may be added to the eluent as  $\text{Na}_2\text{HPO}_4 \cdot 7\text{H}_2\text{O}$ . In the saline eluent it forms  $\text{Na}^+$  and  $\text{PO}_4^{-3} \rightleftharpoons \text{HPO}_4^{-2} \rightleftharpoons \text{H}_2\text{PO}_4^-$ . Upon addition of  $\text{NaOH}$  some of the  $\text{H}_2\text{PO}_4^-$  would be used up in the formation of  $\text{HPO}_4^{-2}$ . The balanced equation being:



When acid is added for example  $\text{HCl}$ ; some  $\text{H}_2\text{PO}_4^-$  is formed. The balanced equation being:



Carbonate salts include water soluble carbonate salts such as alkali metal carbonates and alkali metal hydrogen carbonates for example  $\text{NaHCO}_3$ . In water  $\text{NaHCO}_3$  forms  $\text{Na}^+$  and  $\text{CO}_3^{-2} \rightleftharpoons \text{HCO}_3^- \rightleftharpoons \text{H}_2\text{CO}_3$ . Upon addition of  $\text{NaOH}$ ;  $\text{HCO}_3^-$  and  $\text{H}_2\text{CO}_3$  are used up and  $\text{CO}_3^{-2}$  and  $\text{HCO}_3^-$  respectively are formed. Upon addition of  $\text{HCl}$ ;  $\text{CO}_3^{-2}$  and  $\text{HCO}_3^-$  are used up and  $\text{HCO}_3^-$  and  $\text{H}_2\text{CO}_3$  respectively are formed.

A column containing adsorbant is charged with  $^{82}\text{Sr}$ . Preferably the adsorbant is hydrated tin oxide or polyantimonic acid, and most preferably, hydrated tin oxide. The column is then eluted with the eluent.  
5 Elution rates of 5-10 ml per minute or higher are useful.

At clinically useful flow rates of about 20 ml per minute,  $^{82}\text{Sr}$  breakthroughs of  $10^{-9}$  per ml of eluate are obtained by the present invention. Breakthrough is  
10 the ratio of microcuries of  $^{82}\text{Sr}$  in the eluate to the microcuries of  $^{82}\text{Sr}$  on the adsorber.

$^{82}\text{Rb}$  yields of 90% of theoretical maximum and high radioactive concentration in the eluate (90% elution yield in 5-10 cc) as well as low  $^{82}\text{Sr}$  breakthroughs  
15 of  $10^{-9}$ /ml are obtained using the present invention. These yields may be obtained over a 0.1 minute interval using an eluent flow rate of 30 ml/min.

The procedure used in examples 1-4 is as follows:

50 mg amounts of one of  $\text{Ti}(\text{OH})_4$ , polyantimonic  
20 acid,  $\text{SnO}_2$  (hydrated) or ferric oxide (hydrated) are shaken with 5 ml of liquid phase. The liquid phase is either isotonic saline (0.9%  $\text{NaCl}$ ) or saline and phosphate salt solution. The phosphate concentrations are 0.25% and 0.025%. 0.02 ml of  $\text{Sr-85}$  or  $\text{Rb-83}$  is added.  
25 After one hour of equilibration, 1 ml fractions are pipetted. The activity in each fraction is measured and the  $K_D$  calculated.

The  $\text{SnO}_2$  (hydrated) used in Example 3 is sold by Applied Research, Rue Hercoliers, Brussels, Belgium as oxide d'etain hydrate', (which is French for hydrated tin oxide); OXTAIN (Trademark). This material is a chromatographic amorphous mixture comprising tin oxide and a substantial amount of hydrated stannic oxide. Upon heating, this material loses most of its Sr-Rb separation ability. Thus, there is a loss of activity with the loss of hydration of tin oxide.

Example	Adsorbants	pH	K <sub>D</sub>	
			Sr-82	Rb-82
1	<u>Ti(OH)<sub>4</sub></u>			
	saline (0.9%)	8	40,000	52
	saline + 0.025% PO <sub>4</sub> <sup>-3</sup>	7.8	57,000	54
	saline + 0.25% PO <sub>4</sub> <sup>-3</sup>	8	71,000	56
	saline (0.9%)	2.7	47,500	<3
	saline 0.025% PO <sub>4</sub> <sup>-3</sup>	2.7	114,000	<3
	saline + 0x.25% PO <sub>4</sub> <sup>-3</sup>	4.6	64,000	<3
2	<u>polyantimonite acid</u>			
	saline (0.9%)	7.6	60,000	<3
	saline + 0.025% PO <sub>4</sub> <sup>-3</sup>	7.6	41,000	<3
	saline + 0.25% PO <sub>4</sub> <sup>-3</sup>	7.6	42,000	<3
3	<u>SnO<sub>2</sub> (hydrated)</u>			
	saline (0.9%)	3.6	<3	<3
	saline + 0.025% PO <sub>4</sub> <sup>-3</sup>	4.1	7	<3
	saline + 0.25% PO <sub>4</sub> <sup>-3</sup>	6.5	1.182	<3
4	<u>Fe<sub>2</sub>O<sub>3</sub> (hydrated)</u>			
	saline (0.9%)	3.6	<3	<3
	saline + 0.025% PO <sub>4</sub> <sup>-3</sup>	4.1	7	<3
	saline + 0.25% PO <sub>4</sub> <sup>-3</sup>	6.5	1.182	<3



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In Examples 1-4 the difference in  $K_D$  values for  $^{82}\text{Sr}$  and  $^{82}\text{Rb}$  shows the amount of separation. The high  $K_D$  values for  $^{82}\text{Sr}$  and the low  $K_D$  values for  $^{82}\text{Rb}$  show that  $^{82}\text{Sr}$  is strongly adsorbed while  $^{82}\text{Rb}$  is only slightly adsorbed. Thus, while a Sr loaded column of the adsorbants in Examples 1-4 is eluted the Sr remains adsorbed strongly with very minute breakthrough into the eluate. The daughter  $^{82}\text{Rb}$  is only slightly adsorbed and passes out into the eluate in yields of about 90%.

The bolus volume is the amount of eluent needed to elute the available  $^{82}\text{Rb}$ .

Example 5

Into a column 2 inches long and one fourth inch in diameter is placed 1.5cc of  $\text{SnO}_2$  (hydrated)

particles having diameters of from .05 to 0.1mm.

- 5 Pre-equilibrium is done by washing the  $\text{SnO}_2$  (hydrated) with saline three times. 2 ml of Sr-82 in saline solution having a pH of about 11 is loaded onto the  $\text{SnO}_2$  (hydrated) particles by gravity in about one minute. The column is eluted at 12 ml per minute. The multi scaler mode on a multi-
- 10 channel analyzer was used to determine the elution profile. The bolus volume is about 3.4 ml.

The column is allowed to equilibrate and then counted for 777 KeV(Rb-82) with a Ge(Li) detector.

- 15 Table 1 shows the eluent composition volumes and the breakthrough fraction of  $^{82}\text{Sr}$  for each volume eluted.

- 20 Table 2 shows a Summary of Characteristics of  $^{82}\text{Rb}$  Generator Systems using inorganic adsorbers. At the bottom of the table are shown the characteristics of the  $\text{SnO}_2$  (hydrated) adsorbant of the present invention.

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Table 1  
BREAKTHROUGH OF  $^{82}\text{Sr}$  IN A  $^{82}\text{Rb}$  GENERATOR HAVING A  $\text{SnO}_2$   
(HYDRATED) ADSORBANT

5	Eluent	Volume (CC)	pH Eluate	Fraction of Sr loaded/cc
	NaCl pH9	0 - 150	~1	---
	NaCl pH9	150 - 160	1.5	$7 \times 10^{-6}$
	NaCl pH9	160 - 170	2	$5 \times 10^{-6}$
	NaCl pH9	170 - 200	2	$7 \times 10^{-6}$
10	$\text{Na}_2\text{HPO}_4$			
	0.25%	200 - 205	6.5	$2 \times 10^{-6}$
	"	210 - 250	7	$1.5 \times 10^{-7}$
	$\text{Na}_2\text{HPO}_4$			
	0.025%	250 - 295	7	$9 \times 10^{-8}$
	pH9	295 - 348	7	$7 \times 10^{-8}$
	"	345 - 600	7	$5 \times 10^{-8}$
15	"	600 - 650	7	$10^{-8}$
	"	650 - 700	7	$2 \times 10^{-8}$
	"	700 - 750	7	$2 \times 10^{-8}$
	"	750 - 800	7	$5 \times 10^{-9}$
	"	800 - 850	7	$\leq 5 \times 10^{-9}$
	"	850 - 900	7	$\leq 10^{-8}$
	"	900 - 950	7	$\leq 1.5 \times 10^{-8}$
20	"	950 - 1000	7	$\leq 10^{-8}$
	"	1000 - 1050	7	$\leq 2.5 \times 10^{-8}$
	"	1050 - 1100	7	$\leq 10^{-8}$
	"	1100 - 1150	7	$\leq 2 \times 10^{-8}$
	"	1150 - 1200	7	$\leq 2.5 \times 10^{-8}$
25	"	1200 - 1250	7	$\leq 5 \times 10^{-9}$
	"	1250 - 1300	7	$\leq 2.5 \times 10^{-8}$
	"	1300 - 1350	7	$\leq 3 \times 10^{-8}$
	"	1350 - 1400	7	$\leq 5 \times 10^{-9}$
	"	1400 - 1450	7	$\leq 1.5 \times 10^{-8}$
30	"	1450 - 1800	7	$\leq 5 \times 10^{-9}$
	"	1500 - 1550	7	$\leq 10^{-8}$
	"	1550 - 1600	7	$\leq 1.5 \times 10^{-8}$
	"	1600 - 2100	7.4	$\leq 10^{-8}$
	"	2100 - 3100	7.4	$\leq 5 \times 10^{-10}$
35	"	3100 - 3925		
	"	3925 - 4600	7.4	$1 \times 10^{-9}$
	"	4600 - 5000	7.4	$1 \times 10^{-9}$

In Table I above a " $\leq$ " represents less than or equal to

Table 2  
SUMMARY OF CHARACTERISTICS OF  $^{82}\text{Rb}$  GENERATOR SYSTEMS USING INORGANIC ADSORBERS

Adsorbant	Column Size (ml)	Eluent Used	Elution Speed (ml/sec)	Eluate pH	Rb-82 Yield %	Sr-82 Break-through (ml)	No. Elutions Tested
$\text{Al}_2\text{O}_3$	1	$\text{NaCl}$ 2%	1.2	8-9	70/10 ml	$4 \times 10^{-6}$	250
		$\text{NaCl}$ 0.9%	1.2	8-9	25/10 ml	$5 \times 10^{-6}$	250
$\text{Al}_2\text{O}_3$	2.25	$\text{NaCl}$ 2%	0.5	8-9	76/20 ml	$5 \times 10^{-6}$ - $5 \times 10^{-8}$	300
$\text{Al}_2\text{O}_3$	2.75	$\text{NaCl}$ 0.9%	5	7.5	35/20 ml	-	600
	2.75	$\text{NaCl}$ 0.9%	0.1	7.5	-	$1 \times 10^{-7}$	600
$\text{ZrO}_2$	2.75	$\text{NaCl}$ 0.9%	5	7.5	56/20 ml	-	600
	2.75	$\text{NaCl}$ 0.9%	0.1	7.5	-	$2 \times 10^{-7}$	600
$\text{SnO}_2$ (hydrated) (of the present invention)	1.5	$\text{PO}_4^{3-}$ buffered isotonic saline (pH9)	0.2	7.4	95/4 ml	$\leq 5 \times 10^{-9}$	1,000

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CLAIMS

1. A composition comprising  $^{82}\text{Sr}$  and an adsorbant selected from tin oxide, hydrated tin oxide, polyantimonic acid, titanium oxide, hydrated titanium oxide, ferric oxide and hydrated ferric oxide.
2. The composition of claim 1 wherein said adsorbant is hydrated tin oxide or polyantimonic acid.
3. The composition of claim 1 wherein said adsorbant comprises chromatographic particles of hydrated tin oxide.
4. The composition of claim 3 wherein said particles have an average diameter of 0.01 to 0.9 mm.
5. The composition of claim 3 wherein said particles have an average diameter of 0.05 to 0.1 mm.
6. The composition of claim 3, 4 or 5 wherein said hydrated tin oxide is a substantial amount of hydrated stannic oxide.
7. The composition of claim 6 wherein said composition is amorphous.
8. A low  $^{82}\text{Sr}$  breakthrough method of generating  $^{82}\text{Rb}$  comprising eluting the  $^{82}\text{Rb}$  from the  $^{82}\text{Sr}$  charged adsorbant of any one of claims 1 to 7.
9. The method of claim 8 wherein said  $^{82}\text{Sr}$  charged adsorbant is held in an elutable container means.

10. The method of claim 8 or 9 wherein said eluting is performed with an eluent solution which comprises isotonic saline.

11. The method of claim 10 wherein said eluent solution includes a pharmaceutically acceptable buffer.

12. The method of claim 11 wherein said buffer comprises a phosphate salt or a carbonate salt.